Hydrogen, hydrogen derivatives and e-fuels

















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	Hydrogen Gas	Liquid Hydrogen	Liquid Ammonia (Green Ammonia)	Liquid Methanol (eMethanol)	Dimethylether (eDME)	Liquefied Natural Gas (eLNG)	Synthetic Aviation Kerosene (eSAF)
Ideal universal reaction	Compressed H ₂	Liquefied H ₂	$3H_2 + N_2 \rightarrow 2NH_3$	$3H_2 + CO_2 \rightarrow CH_3OH + H_2O$	$6H_2 + 2CO_2 \rightarrow CH_3OCH_3 + 3H_2O$	$4H_2 + CO_2 \rightarrow CH_4 + 2H_2O$	$10CO_2 + 31H_2 \rightarrow C_{10}H_{22} + 20H_2O$
Hydrogen yield	100 %	100 %	100 %	4/6 = 67 %	6/12 = 50 %	4/8 = 50 %	22/62 = 35.5 %
Ideal conversion energy	100 %	100 %	88,7 %	92,3 %	91,7 %	82,9 %	84,0 %
efficiency*							
Reaction temperature °C**	50-80	50-80	350-550	200-300	200-300	300-400	180-250
Volumetric energy	2.43 - 6.8	8.52	12.7	15.7	18.7 Liquefied gas at 20°C	22.2	35
density, LHV (MJ/L)							
Gravimetric energy density,	120	120	18.6	19.9	28.4 Liquefied gas at 20°C	48.6	42.2
LHV (MJ/kg)							
Infrastructure readiness for	Low	Low	High	High	High	High	High
large scale deployment in							
mid-term							
Transportation and	Ambient	-253 °C	-33.3 °C	Liquid at ambient	Liquefied gas at 4.2 bar 20°C	-162 °C	Ambient
storage temperature				temperature			
Transportation and storage	Compressed gas	Liquid at amos-	Liquid at amos-	Liquid at amospheric	Liquefied gas at 4.2 bar 20°C	Liquid at amospheric	Liquid at amospheric
phase and pressure	at 250 to 700 bar	pheric pressure	pheric pressure	pressure		pressure	pressure
Density	0.017 kg/L	0.071 kg/L	0.68 kg/L	0.79 kg/L	0.66 kg/L Liquefied gas at 20°C	0.46 kg/L	0.83 kg/L
Toxicity	Non toxic	Non toxic	TWA 25 ppm	TWA 200 ppm	TWA 1,000 ppm	TWA 1,000 ppm	TWA 30 ppm
Flammability (% in air)	4-74%	4-74%	14.8 - 33.5 %	6.0 - 36.5 %	3.4 - 18 %	4 - 15 %	0.7 - 4.8 %

Notes

^{*} Ideal stoichiometric reaction energy conversion with no heat losses (LHV fuel / LHV H₂ feed)

^{**} Approximate temperature range at which waste heat is liberated for direct use or steam generation