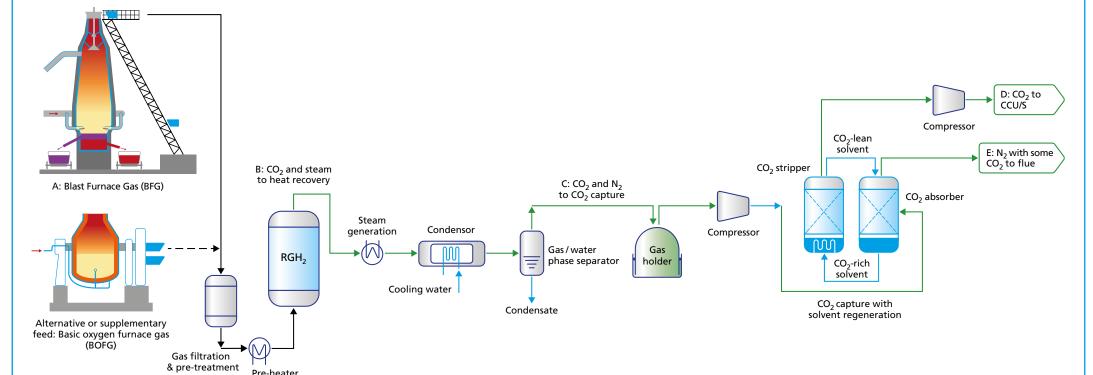
## Stage 1 (BFG and / or BOFG feedstock): Reduction and CO<sub>2</sub> recovery. Reduction of the RGH<sub>2</sub> oxygen-carrier with CO, H<sub>2</sub> and CH<sub>4</sub> from iron and steel making flue gases.

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Stream	CO <sub>2</sub> Mol%	<b>H₂</b> Mol%	CO Mol%	N <sub>2</sub> Mol%	H₂O Mol%	<b>Temp</b> °C
A: Blast Furnace Gas to RGH <sub>2</sub>	22	4	24	50	0	50
B: CO <sub>2</sub> , N <sub>2</sub> and steam from RGH <sub>2</sub>	46	0	0	50	4	770
C: CO <sub>2</sub> and N <sub>2</sub> to CO <sub>2</sub> capture	46	0	0	50	4	50
D: CO <sub>2</sub> to utilisation or sequestration	97	0	0	0	3	100
E: Nitrogen and CO <sub>2</sub> slip to flue****	5	0	0	92	3	<b>Ambient</b>

## Key reactions in the RGH<sub>2</sub> plug-flow, iron-oxide chemical looping reactor

$$3Fe_2O_3 + H_2 \rightarrow 2Fe_3O_4 + H_2O^*$$
  
 $3Fe_2O_3 + CO \rightarrow 2Fe_3O_4 + CO_2^*$ 

$$2Fe_3O_4 + 2H_2 \leftrightarrow 6FeO + H_2O^{**}$$
  
 $2Fe_3O_4 + 2CO \leftrightarrow 6FeO + 2CO_2^{**}$ 

$$6\text{FeO} + 6\text{H}_2 \leftrightarrow 6\text{Fe} + 6\text{H}_2\text{O}^{***}$$

6Fe0 + 6CO ↔ 6Fe + 6CO<sub>2</sub>\*\*\*

- \* This reaction non-reversible is required to ensure full conversion of H<sub>2</sub> and CO in the syngas feed to CO<sub>2</sub> and moisture.
- \*\* This reversible reaction converts 65 to 80% of hydrogen and CO in the syngas feed to CO<sub>2</sub> and moisture.
- \*\*\* This reversible reaction converts 30 to 40% of hydrogen and CO in the syngas feed to CO2 and moisture.

<sup>\*\*\*\*</sup> Composition shown is indicative of solvent-based CO<sub>2</sub> capture plants operating at a reasonable balance of CO<sub>2</sub> capture rate and energy efficiency).